

Supporting Information

The formulas used for hot water production system equipment are as follows:

a) For the compressor: [1, 2]

$$\dot{E}x_D = \dot{E}x_F - \dot{E}x_P = \quad (7)$$

$$\sum (\dot{m}.e)_{in} + W - \sum (\dot{m}.e)_{out}$$

$$\varepsilon = \frac{\sum (\dot{m}.e)_{in} - \sum (\dot{m}.e)_{out}}{W} \quad (8)$$

b) For condensers, evaporators, and heat exchangers: [3]

$$\dot{E}x_D = \dot{E}x_F - \dot{E}x_P = \quad (9)$$

$$\left[\sum (\dot{m}.e) \right]_{in,(Hot)} + \left[\sum (\dot{m}.e) \right]_{1,(Cold)} - \left[\sum (\dot{m}.e) \right]_{out,(Hot)} - \left[\sum (\dot{m}.e) \right]_{2,(Cold)}$$

$$\varepsilon = \frac{[\sum (\dot{m}.e)]_{in,(Hot)} - [\sum (\dot{m}.e)]_{out,(Hot)}}{[\sum (\dot{m}.e)]_{2,(Cold)} - [\sum (\dot{m}.e)]_{1,(Cold)}} \quad (10)$$

c) For solar collectors: [2-6]

$$\dot{E}x_D = \dot{E}x_F - \dot{E}x_P = \quad (11)$$

$$\sum (\dot{m}.e)_{in} + Q \left(1 - \frac{T}{T_0} \right) - \sum (\dot{m}.e)_{out}$$

$$\varepsilon = \frac{Q(1 - \frac{T}{T_0})}{\sum (\dot{m}.e)_{in} - \sum (\dot{m}.e)_{out}} \quad (12)$$

d) for pump: [2-6]

$$\dot{E}x_D = \dot{E}x_F - \dot{E}x_P = \quad (13)$$

$$\sum (\dot{m}.e)_{in} + W - \sum (\dot{m}.e)_{out}$$

$$\varepsilon = \frac{\sum (\dot{m}.e)_{in} - \sum (\dot{m}.e)_{out}}{W} \quad (14)$$

e) For pressure relief valve: [2-5]

$$\dot{E}x_D = \dot{E}x_F - \dot{E}x_P = \quad (15)$$

$$\sum (\dot{m}.e)_{in} - \sum (\dot{m}.e)_{out}$$

$$\varepsilon = \frac{e_{out}^{\Delta T} - e_{in}^{\Delta T}}{e_{out}^{\Delta P} - e_{in}^{\Delta P}} \quad (16)$$

A detailed sensitivity analysis of the parameters used in the study is presented in Figs 12 to 18.

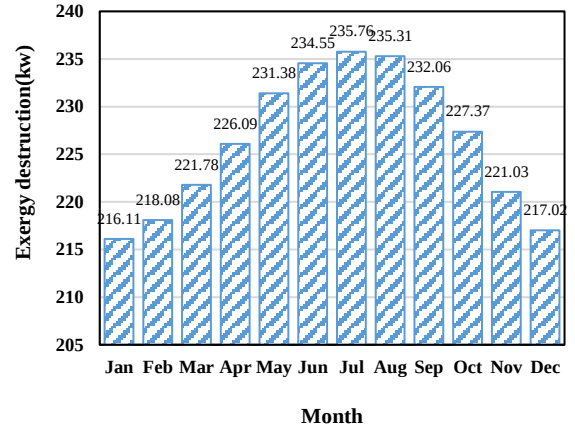


Fig. 12: Exergy destruction (kW) Compressor 1

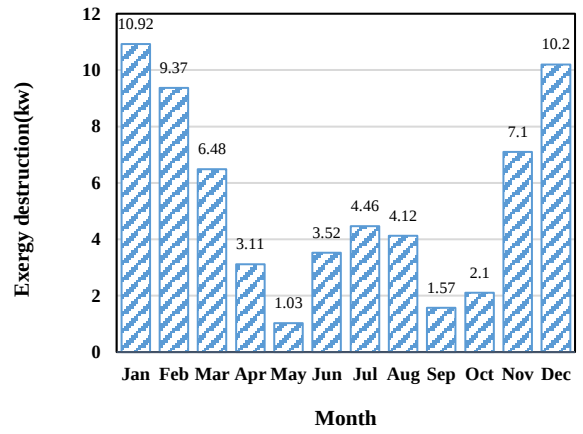


Fig. 13: Exergy destruction (kW) Heat Exchanger 2.

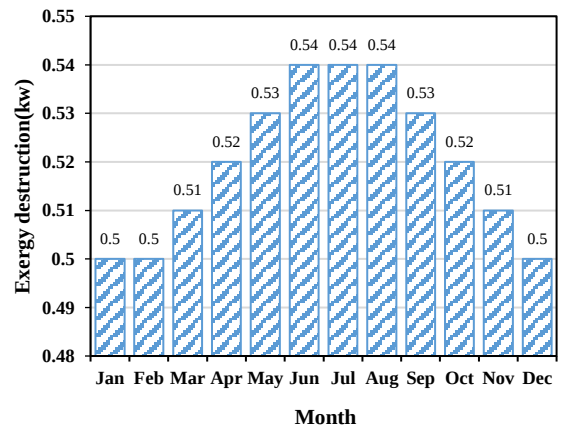


Fig. 14: Exergy destruction (kW) Pump 1

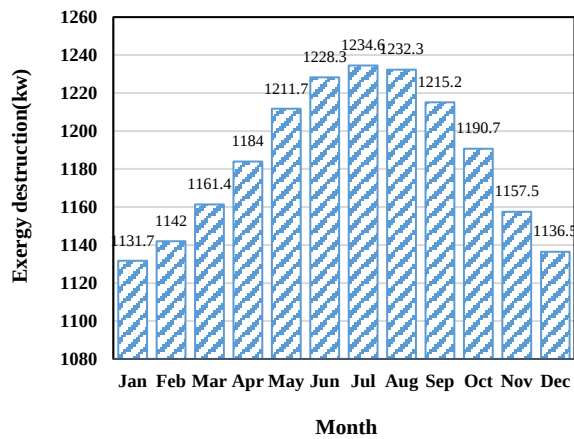


Fig. 15: Exergy destruction (kW) Heat Exchanger 1.

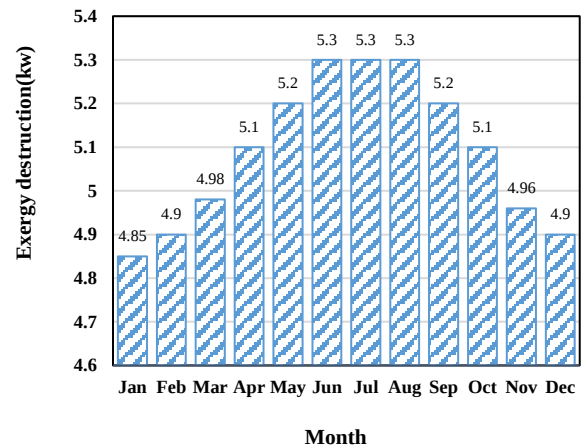


Fig. 17: Exergy destruction (kW) Expansion Valve.

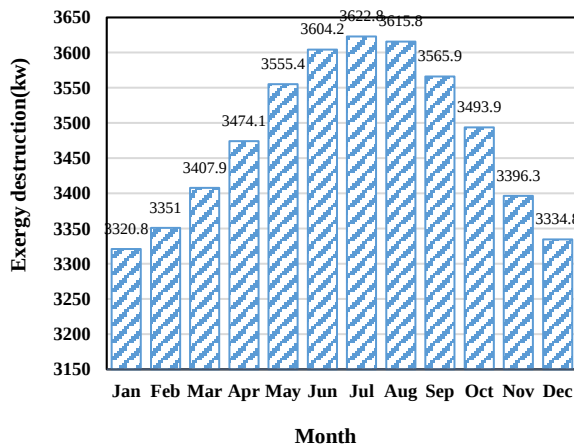


Fig. 16: Exergy destruction (kW) Storage Tank.

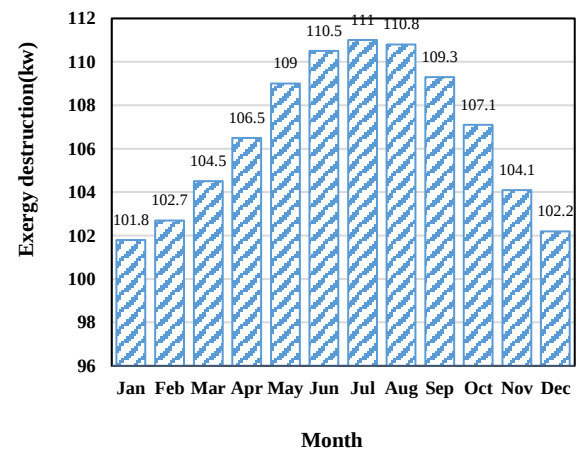


Fig. 18: Exergy destruction (kW) Expander.

Reference

- [1] Mehrpooya M., Shafaei A., [Advanced Exergy Analysis of Novel Flash Based Helium Recovery from Natural Gas Processes](#), *Energy*, **114**: 64-83 (2016).
- [2] Vatani A., Mehrpooya M., Palizdar A., [Advanced Exergetic Analysis of Five Natural Gas Liquefaction Processes](#), *Energy Conversion and Management*, **78**:720-737 (2014).
- [3] Ghorbani B., Salehi G., Ghaemmaleki H., Amidpour M., Hamed M., [Simulation and Optimization of Refrigeration Cycle in NGL Recovery Plants with Exergy-Pinch Analysis](#), *Journal of Natural Gas Science and Engineering*, **7**: 35-43 (2012).
- [4] Mehrpooya M., Lazemzade R., Sadaghiani M.S., Parishani H., [Energy and Advanced Exergy Analysis of an Existing Hydrocarbon Recovery Process](#), *Energy Conversion and Management*, **123**:523-534 (2016).
- [5] Ghorbani B., Shirmohammadi R., Mehrpooya M., [A Novel Energy Efficient LNG/NGL Recovery Process Using Absorption and Mixed Refrigerant Refrigeration Cycles–Economic and Exergy Analyses](#), *Applied Thermal Engineering*, **132**:283-295 (2018).
- [6] Kelly S., ["Energy Systems Improvement Based on Endogenous and Exogenous Exergy Destruction"](#) (2008).